Focused Cross Flow LBE Target for ESS

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2003 reference design for a mercury target

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Focused Cross Flow Target

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2003 reference design for a mercury target





2003 reference design for a mercury target

boundary conditions

- ➤ 5 MW beam power / ~2.9 MW heat deposition (incl. 20% safety margin)
- ≻ 50 Hz pulse frequency
- ≻1.4 µs pulse length
- ≻1.334 GeV proton energy
- elliptical beam footprint (200mm x 60mm)
- ➤ parabolic beam profile
- 175 kg/s mercury flow
 (best operating conditions for
 15% of total mass flow rate through bottom inlet duct)
- ➤ 100 °C inlet temperature
- ➤ ~220 °C mean outlet temperature
 - $\Delta T_{window} \cong 7 \text{ K / pulse}$
 - \blacktriangleright $\Delta T_{Hg} \simeq 37 \text{ K} / \text{pulse}$



elliptical beam footprint





2003 reference design for a mercury target

Flow instabilities (transient effects and effects due to slightly unsymmetric inlet conditions) can lead to zones of high temperatures in the bulk outlet region of the target, alternately touching the walls



257

205

152

left: stationary calculation performed for a halfmodel showing stable vortices in the front part right: transient calculation performed for a fullmodel showing strong fluctuations

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left: transient calculation for perfectly symmetric inlet conditions

right: transient calculation for unsymmetric inlet conditions (mass flow rate suddenly increased by 2% for right and decreased by 2% for the left side duct)

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time scale of the long-pulse (2 ms) is still small compared to inertia effects of the target material in the rear end of the target

>thermal expansion of the target material is compensated by local compression of the material itself and a local expansion of the target container in the front part

>expansion of target container may lead to significant stresses in the window region

stressing of the target window for a mercury long-pulse target at $16^{2}/_{3}$ Hz

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 \Rightarrow same pressure drop can be expected for a mass flow rate of:

LBE as preferred target material for a liquid metal target

- heat removal capability is comparable: \Rightarrow
- \Rightarrow heat transfer coefficients are comparable: (e.g. formulas for turbulent pipe flow, $d \approx 100$ mm):

but

- to avoid solidification of LBE, the inlet temperature must be si higher: 175 – 200°C (> 125°C) for LBE instead of 100°C for mercury
- no risk of evaporation (evaporation temperature is 1670°C for LBE) instead of 357°C for mercury)

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Changes to boundary conditions LBE as preferred liquid metal

$$\dot{m}_{LBE} = \dot{m}_{Hg} \sqrt{\frac{\rho_{LBE}}{\rho_{Hg}}} = 155 \frac{kg}{s}$$

$$\frac{\dot{m}_{LBE} \cdot c_{p_{LBE}}}{\dot{m}_{Hg} \cdot c_{p_{Hg}}} = 0.95$$

$$\frac{\alpha_{LBE}}{\alpha_{Hg}} = 1.084$$

proton energy and beam profile

 $higher proton energy \Rightarrow reduced power density in the front part$

Power density along the beam axis for Hg with 1.334 GeV protons and LBE with 2.5 GeV protons, both for 2.3 MW heat deposition

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proton energy and beam profile

 \Im Gaussian beam profile with $\pm \kappa_{\sigma} \cdot \sigma$ within the beam footprint

- \Rightarrow peak power density will be increased by $\kappa_{\sigma}^{2}\!/\!4$
- \Rightarrow energy outside of elliptical beam footprint: $e^{-0.5 \kappa_{\sigma}^2}$ of total thermal energy (has to be removed by collimator)

left: radial distribution of rel. power density for different Gaussian profiles right: rel. peak power density and heat loss for different Gaussian Profiles

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 decreased pulse frequency will increase the energy per pulse and therefore the temperature increment per pulse in the structure and fluid
 maximum values for a Gaussian beam profile and κ_σ=2

 \Rightarrow short pulse (1.4 µs) \Rightarrow long pulse (2 ms)

for the long pulse target the risk of cavitation damage is significantly reduced
 compared to the short pulse target

completely compressed thermal expansion of fluid ∜pressure pulse only depends ´ on total energy per pulse and not on the pulse length

sudden change in heating rate
will cause a pressure pulse at the
beginning (positive) and the end
(negative) of each proton pulse
♥ pressure pulse strongly
depends on pulse length

♥ concept

>Main concept of the 'focused cross flow design':

- cross flow design for same container geometry than 2003 reference target
- inclined horizontal plates accelerate the flow in the horizontal midplane
- flow pattern in the critical zones is adjusted by curvature and variable spacing of baffles (in order to generate a certain pressure drop for each 'channel')

updated boundary conditions

*left: power density for LBE during pulse in W/m*³

right: assumed power density for steel during pulse in W/m³ (scaled by density)

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by pros and <u>cons</u>

> additional structural material within the zone of high heat deposition

left: power density in structural material for the focused cross flow target right: power density in structural material for the 2003 target design

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by pros and <u>cons</u>

> window cooling inferior to 2003 reference design

left: structural temperatures for focused cross flow target right: structural temperatures for the 2003 target design

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✤ pros and cons

> more reliable flow pattern and consequently more reliable heat removal

Iess temperature fluctuations close to the container walls

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✤ pros and cons

more reliable flow pattern and consequently more reliable heat removal

less temperature fluctuations close to the walls

fluid temperatures for focused cross flow target

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left: fluid velocity for focused cross flow target right: fluid velocity for the 2003 target design

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left: absolute pressure; pressure drop: $\Delta p \cong 0.3$ *bar* *right: absolute pressure; pressure drop:* $\Delta p \cong 1.9$ bar

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Preliminary Conclusions & Outlook

- The focused cross flow target has still some potential for optimization with respect to window cooling and heat removal capability (e.g. baffle arrangement, increased mass flow rate)
- Solution Window cooling and heat removal in the zone of maximum power density seems to be already sufficient for a 5MW proton beam

Outlook

- Temperature and velocity limits have to be defined for the target
 Further optimization of flow field
- Evaluation of thermal and mechanical stresses in the target (e.g. stresses due to pulsed operation, possible thermal striping, ...)
- Producibility aspects have to be clarified

> LBE as preferred target material for a liquid metal target

 \Rightarrow same pressure drop can be expected for a mass flow rate of

$$\dot{m}_{LBE} = \dot{m}_{Hg} \sqrt{\frac{\rho_{LBE}}{\rho_{Hg}}} = 155 \frac{kg}{s}$$

(effect of viscosity neglected)

 \Rightarrow heat removal capability is comparable:

$$\frac{\dot{m}_{LBE} \cdot c_{p_{LBE}}}{\dot{m}_{Hg} \cdot c_{p_{Hg}}} = \frac{155 \frac{kg}{s} \cdot 146 \frac{J}{kg \cdot K}}{175 \frac{kg}{s} \cdot 136 \frac{J}{kg \cdot K}} = 0.95$$

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⇒ heat transfer coefficients are comparable: (e.g. formulas for turbulent pipe flow, d \cong 100mm)

$$\frac{\alpha_{LBE}}{\alpha_{Hg}} = \frac{\frac{(1.8 \cdot \log(\operatorname{Re}_{LBE}) - 1.5)^{-2}}{8} \cdot \operatorname{Re}_{LBE} \cdot \operatorname{Pr}_{LBE}}{\frac{1 + 12.7 \cdot \sqrt{\frac{(1.8 \cdot \log(\operatorname{Re}_{LBE}) - 1.5)^{-2}}{8}} \cdot \left(\operatorname{Pr}_{LBE}^{\frac{2}{3}} - 1\right)}}{\frac{(1.8 \cdot \log(\operatorname{Re}_{Hg}) - 1.5)^{-2}}{8} \cdot \operatorname{Re}_{Hg} \cdot \operatorname{Pr}_{Hg}}{\frac{1 + 12.7 \cdot \sqrt{\frac{(1.8 \cdot \log(\operatorname{Re}_{Hg}) - 1.5)^{-2}}{8}} \cdot \operatorname{Re}_{Hg} \cdot \operatorname{Pr}_{Hg}}{1 + 12.7 \cdot \sqrt{\frac{(1.8 \cdot \log(\operatorname{Re}_{Hg}) - 1.5)^{-2}}{8}} \cdot \left(\operatorname{Pr}_{Hg}^{\frac{2}{3}} - 1\right)}} \cdot \left(\operatorname{Pr}_{Hg}^{\frac{2}{3}} - 1\right)}$$

thermal-hydraulic design is similar for mercury and LBE

but

Sto avoid solidification of LBE, the inlet temperature must be significantly higher: 175 – 200 °C (> 125°C) for LBE instead of 100°C for mercury

Sho risk of evaporation (evaporation temperature of 1670 °C for LBE instead of 357 °C for mercury) 4th HPTW J. Wolters and M. Butzek, Central Department of Technology slide 23/21